

Fluid Mechanics.

11/12 Sem I

CV 2601.

1. (a)  $v = 5 \text{ m/s}$ ,  $y = 2 \times 10^{-3}$ ,  $\mu = 0.01$

$$\tau = \mu \frac{\partial u}{\partial y}$$

$$= \mu \cdot \frac{v}{y}$$

$$= 0.01 \times 5 \times \frac{1}{2 \times 10^{-3}}$$

$$= 25 \text{ Pa.s}$$

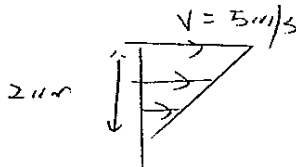
$$\therefore \frac{dw}{dt} = F \cdot v$$

$$P = F \cdot v$$

$$= 50 \times 5$$

$$= 250 \text{ J/s}$$

○  $\therefore F = \tau \times A$   
 $= 25 \times 2 \times 1$   
 $= 50 \text{ N}$



Ans: The power against fluid shear stress is 250 J/s.

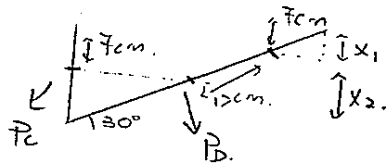
b)  $\Delta \rho = 995.7 - 1000$   
 $= -4.3 \text{ kg/m}^3$

$$\therefore \Delta p = K \cdot \frac{\Delta \rho}{\rho_0}$$

$$= 215 \times 10^7 \times \frac{4.3}{1000}$$

$$= 9245000 \text{ Pa}$$

○ Ans: The applied pressure is 9245000 Pa.



$$\tan 30^\circ = \frac{7}{x}$$

$$\therefore x = \frac{7}{\tan 30^\circ}$$

$$P_C = P_D$$

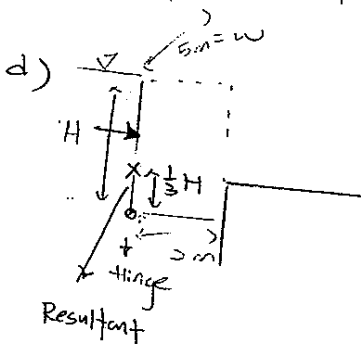
$$P_A + \rho_0 g h = P_B + \rho_{oil} g x_1 + \rho_{mercury} g x_2$$

$$5 \times 10^3 + 13.6 \times 10^3 \times 9.81 \times \frac{7}{100} = P_B + 0.87 \times 10^3 \times 9.81 \times \frac{7}{\tan 30^\circ} \times \frac{1}{100} + 13.6 \times 10^3 \times 9.81 \times \frac{12}{\tan 30^\circ} \times \frac{1}{100}$$

$$P_B = -23.078 \text{ kPa}$$

$$= -23.078 \text{ kPa}$$

Ans: The pressure at B is  $-23.078 \text{ kPa}$ .



$F_H$  = weight of the volume prism

$$F_H = \rho g H \times H \times 5 \times \frac{1}{2}$$

$$= \frac{5}{2} \rho g H^2 \quad (\rightarrow)$$

The  $F_H$  is acting at  $\frac{1}{3} H$  from the hinge.

$$F_V = \rho g H \times 2 \times 5$$

$$= 10 \rho g H \quad (\uparrow)$$

The  $F_V$  will act on 1 m left from hinge.

$\therefore$  The gate is in equilibrium;

$$\therefore \sum M_{\text{hinge}} = 0$$

$$\frac{1}{3} H \times \frac{5}{2} \rho g H^2 = 10 \rho g H \times 1$$

$$\frac{5}{6} \rho g H^3 = 10 \rho g H$$

$$\frac{5}{6} H^3 - 10 H = 0$$

$$H \left( \frac{5}{6} H^2 - 10 \right) = 0$$

$$\therefore H = \sqrt{12}$$

$$= 2\sqrt{3} \text{ m}$$

Ans: The height of H is  $2\sqrt{3} \text{ m}$ .

1 e)

$$b = h = 8$$

$$I_{yy} = \frac{1}{12} bh^3$$

$$= \frac{1}{12} 8 \cdot 8^3$$

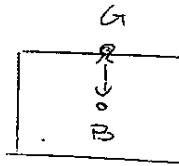
$$= \frac{1024}{3} \text{ m}^4$$

$$V_i = 3 \times 8 \times 8$$

$$= 64 \times 3$$

$$= 192 \text{ m}^3$$

$$\bullet \text{ BG} = 1.5 \text{ m.}$$



$$\bullet \text{ BM} = \frac{I_{yy}}{V_i}$$

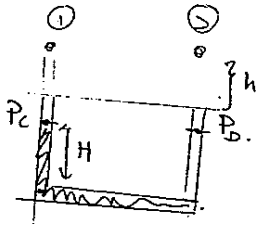
$$= \frac{1024}{192} \times \frac{1}{3}$$

$$= \frac{16}{9} = 1.7778 \text{ m.}$$

$$\therefore \text{ BM} > \text{ BG.}$$

Hence the barge floating is in stable equilibrium.

2(a)



$$\therefore P_1 + \rho_{\text{Mercury}} \times g \times H = P_2 + \rho_{\text{water}} \times g \times H$$

$$\therefore P_1 = P_2 + 1000 \times 9.81 \times \frac{10}{100} - 13.6 \times 1000 \times 9.81 \times \frac{10}{100}$$

$$= P_2 - 12360.6$$

$$\therefore P_1 + \rho g h = P_2 + \rho g h$$

$$P_1 = P_2$$

$$\therefore P_1 = P_2 - 12360.6$$

By Bernoulli Equation.

$$\therefore \frac{P_1}{\rho g} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + z_2$$

$$\therefore z_1 = z_2$$

$$V_2 = 0$$

$$\frac{V_1^2}{2g} + \frac{P_1}{\rho g} = \frac{P_2}{\rho g}$$

$$\therefore \frac{V_1^2}{2g} = \frac{P_2 - P_1}{\rho g}$$

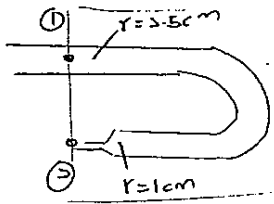
$$V_1^2 = \frac{2(P_2 - P_1)}{\rho}$$

$$= \frac{2 \times 12360.6}{1000}$$

$$V_1 = 4.972 \text{ m/s}$$

Ans: The velocity of the water is 4.972 m/s.

2 (b)



control volume.  $A_2 V_2 = A_1 V_1$ .  
By continuity eqn.

$$V_2 = \frac{A_1 V_1}{A_2} = \frac{\pi D_1^2}{\pi D_2^2} V_1$$

$$\therefore V_2 = \frac{5^2}{2^2} \times 5 = \frac{5^3}{4} \text{ m/s}$$

By using Bernoulli eqn.

$$E_1 = E_2 \quad (\because \text{There is no head loss}).$$

$$\frac{P_1}{\rho g} + z_1 + \frac{V_1^2}{2g} = \frac{P_2}{\rho g} + z_2 + \frac{V_2^2}{2g}$$

$$z_1 = z_2, P_2 = 0.$$

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} = \frac{V_2^2}{2g}$$

$$\frac{P_1}{\rho} = \left[ \frac{5^3}{4} \right]^2 \times \frac{1}{2} - \frac{5^2}{2}$$

$$P_1 = 475.78125 \times 1000$$

$$= 475781.25 \text{ Pa.}$$

Define  $\rightarrow$  (Right) as positive

$$\therefore F_{\text{net}} = M_{\text{out}} - M_{\text{in}}$$

$$= -\rho A_2 V_2^2 - \rho A_1 V_1^2.$$

$$= -\rho \left[ \pi \times 1^2 \times \left( \frac{5^3}{4} \right)^2 + \pi \times 2.5^2 \times 5^2 \right]$$

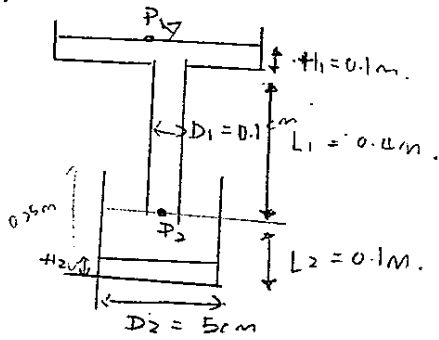
$$= -\rho \pi [945.3125]$$

$$= -2969.7869 \text{ kN} (\rightarrow)$$

• Force acting on fluid  $\Rightarrow$  Right  $\therefore$  Force acting on pipe  $\Rightarrow$  left.

Ans: The hydrodynamic force acting on the horizontal bend is 2969.7869 kN to the left.

3.



$$\begin{aligned} \sum h_L &= \text{entrance loss} + \text{friction loss} \\ &= 0.5 \frac{V_2^2}{2g} + f \frac{L}{D} \frac{V_2^2}{2g} \end{aligned}$$

$$= \left[ 0.5 + \frac{0.2 \times 0.4}{0.1 \times 10^{-2}} \right] \frac{V_2^2}{2g}$$

$$= 80.5 \frac{V_2^2}{2g}$$

a). By using Bernoulli eqn from pt ① to pt ③.

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + z_2 + \sum h_L$$

$$\therefore P_1 = 0, V_1 = 0, P_2 = 0, z_2 = 0, z_1 = 0.5$$

$$0.5 = \frac{V_2^2}{2g} + 80.5 \frac{V_2^2}{2g}$$

$$= 81 \frac{V_2^2}{2g}$$

$$\therefore V_2^2 = \frac{1 \times 9.81}{81}$$

$$V_2 = 0.348 \text{ m/s.}$$

\(\therefore\) The water flow out from the pipe will go into the <sup>container</sup> tank.

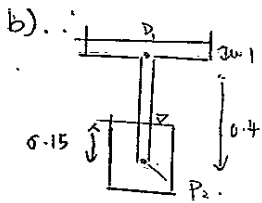
$$\therefore A_2 V_2 = A_3 V_3$$

$$\frac{\pi \cdot D_1^2}{4} \times 0.348 = \frac{\pi \cdot D_2^2}{4} \times V_3$$

$$\therefore V_3 = \frac{0.1^2}{5^2} \times 0.348$$

$$= 1.392 \times 10^{-4} \text{ m/s.}$$

Ans: The rate of the water rising within the container is  $1.392 \times 10^{-4} \text{ m/s.}$



By using Bernoulli eqn.

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + z_2 + \Delta h_L$$

$$z_1 = 0.5, z_2 = 0, P_1 = 0, P_2 = -\rho g \times 0.15$$

$$0.5 = 0.15 + \frac{V_2^2}{2g} + 81 \frac{V_2^2}{2g}$$

$$0.35 = 82 \frac{V_2^2}{2g}$$

$$V_2^2 = \frac{0.35 \times 2}{82}$$

$$V_2 = 0.09239 \text{ m/s}$$

$$\therefore A_2 V_2 = A_3 V_3$$

$$V_3 = \frac{0.1^2}{5^2} \times 0.09239$$

$$= 3.6956 \times 10^{-5} \text{ m/s}$$

Ans: The rate of rise of the water surface is  $3.6956 \times 10^{-5} \text{ m/s}$ .

c)

It consists of two stage for the water to fill up the container.

I. water level  $< 0.1 \text{ m} \rightarrow$  Rate of  $h$  rising  $= 1.392 \times 10^{-4} \text{ m/s}$ .

II water level  $> 0.1$ .  $\rightarrow$  Rate of  $h$  rising  $\Rightarrow$  keep on changing.

$$\text{at } h = 0.25$$

$$V = 3.6956 \times 10^{-5} \text{ m/s}$$

$$\therefore \text{For } h = 0.1 \text{ m}, t_1 = \frac{0.1}{1.392 \times 10^{-4}} = 718.39 \text{ s}$$

$0.1 < h < 0.25$ , we assume the velocity change is linear,  $V_c^2 = \frac{2 \times 9.81 \times 0.5}{82} \times \frac{0.1^2}{5^2}$

$$\therefore \bar{V} = \frac{1.392 \times 10^{-4} + 3.6956 \times 10^{-5}}{2}$$

$$= 8.8078 \times 10^{-5} \text{ m/s}$$

$$V_c = 0.3480 \text{ m/s} \times \frac{0.1^2}{5^2}$$

$$= 1.392 \times 10^{-4} \text{ m/s}$$

$$\text{For } h = 0.15 \text{ m}, t_2 = \frac{0.15}{8.8078 \times 10^{-5}} = 1703.03 \text{ s}$$

$$\therefore T_{\text{total}} = t_1 + t_2 = 718.39 + 1703.03$$

$$= 1881.42 \text{ s}$$

Ans: The total time taken for the container to fill up is  $1881.42 \text{ s}$ .

d)

No. It won't affect the filling time significantly as for the head losses = entrance + pipe + exit losses. The <sup>the water pipe flow losses</sup> component contribute the most significant effect toward the rate of filling. Hence, the changing edge of the entrance will not affect the filling time significantly. as it only contribute a little of head loss in this condition.



4(a).

∴  $\omega$  increased to 3500 rpm.

$$\frac{Q_m}{\omega_m D_m^3} = \frac{Q_p}{\omega_p D_p^3} \quad \therefore D_m = D_p$$

$$\frac{gh_m}{\omega_m^2 D_m^4} = \frac{gh_p}{\omega_p^2 D_p^4}$$

$$\therefore Q_p = \frac{3500}{1750} \times 0.1$$

$$= 2 \times 0.1$$

$$= 0.2 \text{ m}^3/\text{s}$$

$$\frac{h_m}{\omega_m^2} = \frac{h_p}{\omega_p^2}$$

$$\therefore \frac{h_p}{3500^2} = \frac{h_m}{1750^2}$$

$$\therefore h_p = 15 \text{ m} \times 4^2$$

$$= 60 \times 4$$

$$= 240 \text{ m}$$

Ans: The flow rate is  $0.2 \text{ m}^3/\text{s}$  and the head is 240 m.

b)

I) For the shaft:



$$\therefore \sum F = ma$$

$$F_h - F_e = ma$$

We can explain this via Newton's Second law. Assuming only these 2 forces act on the shaft.

when  $a \neq 0$ .

$$F_h = F_e + ma$$

$$\therefore F_h \neq F_e$$

when  $a = 0$ , constant velocity.  
 $v = \text{const}$   
 $\omega = \text{const}$

$$\therefore a = r\omega^2$$

$$\therefore F_h - F_e = 0$$

$$F_h = F_e$$

• Ans:  $F_h = F_e$  only when the shaft is rotating in constant velocity.

$$\text{II) } F_h = f(L, D_1, D_2, \mu, \omega)$$

$\therefore F_h$  is a relationship between  $D_1, D_2, \mu$  and  $L$ .

$$F_h = \frac{\text{kg} \cdot \text{m}}{\text{s}^2} \Rightarrow \frac{ML}{T^2}$$

$$\omega = \text{rads}^{-1} \Rightarrow \frac{1}{T}$$

$$L = \text{m} \Rightarrow L$$

$$D_1, D_2 \Rightarrow L$$

$$\mu \Rightarrow \frac{ML}{T}$$

$$\begin{aligned} \therefore k-r &= 6-3 \\ &= 3 \text{ } \pi \text{ group} \end{aligned}$$

choosing  $L, \mu, \omega$  as repeating units. (In order to construct a relationship between the rest of the unknown with  $D_1, D_2$  and  $F_h$ ).

$$* \frac{ML}{T^2} = L^a \left(\frac{ML}{T}\right)^b \left(\frac{1}{T}\right)^c$$

For  $\pi_1$

$$L: a+b=1$$

$$\frac{1}{T}$$

$$\therefore \pi_1 = \frac{F_h}{\mu \omega}$$

$$T: -b-c = -2$$

$$M: b=1$$

$$\therefore a = 1-1$$

$$= 0$$

$$\therefore -b-c = -2$$

$$-1-1 = c$$

$$\therefore c = 1$$

For  $\pi_2$

$$L = L^a \left(\frac{ML}{T}\right)^b \left(\frac{1}{T}\right)^c$$

$$\pi_2 = \frac{D_1}{L}$$

$$\therefore b=0, c=0$$

$$\therefore a=1$$

For  $\pi_3$

$$L = L^a \left(\frac{ML}{T}\right)^b \left(\frac{1}{T}\right)^c$$

$$\pi_3 = \frac{D_2}{L}$$

$$\therefore a=1$$

Ans: The established relationship is shown as below.

$$\therefore \frac{F_h}{\mu \omega} = \left(\frac{D_1}{L}, \frac{D_2}{L}\right)$$

III) Since the assumption of linear velocity of  $Z$ ,  $\therefore D_2 = 2D_1$ .

$$\frac{D_2 - D_1}{2} - \frac{D_1}{2} = 0.$$

$$\frac{F_u}{u.w} = \phi\left(\frac{D_1}{L}, \frac{D_2}{L}\right)$$

$$\frac{D_2}{2} - \frac{D_1}{2} - \frac{D_1}{2} = 0.$$

$$\frac{D_2}{2} = D_1$$

$$\therefore D_2 = 2D_1.$$

$$\therefore \frac{F_u}{u.w} = \phi\left(\frac{2D_1}{L}, \frac{D_1}{L}\right) \text{ (As they can have a } k \text{ to represent these } \rightarrow \text{ similar } \Pi \text{ group.)}$$
$$= \phi\left(\frac{D_1}{L}\right).$$

$$\therefore \frac{F_u}{u.w} = k \frac{D_1}{L}.$$

$$\therefore F_u = \frac{k u w D_1}{L}.$$

Ans:  $F_u = k \cdot \frac{u w D_1}{L}$ .

IV) If the assumption of linear velocity gradient is no longer valid. Then, we have to establish more relationship between these factor by assuming one of the factor is constant, then establish another relationship between these factor. By experimenting these during experiment, we can find out the relationship of  $F_u$  with these factors.